

Corrections

New Loading Technique for a Vibrating Tube Densimeter and Measurements of Liquid Densities up to 39.5 MPa for Binary and Ternary Mixtures of the Carbon Dioxide–Methanol–Propane System.
L. A. Galicia-Luna, D. Richon,* and H. Renon, *J. Chem. Eng. Data* 1994, 39, 424.

Tables 10 and 14 were incorrectly aligned. The correct tables are printed below.

Table 10. Density ρ of Liquid Ethylene (1)–4-Methyl-1-pentene Liquid System as a Function of Pressure P and Mole Fraction $z(1)$ at Four Temperatures

$P/(\text{MPa})$	$\rho/(10^3 \text{ kg/m}^3)$					$P/(\text{MPa})$	$\rho/(10^3 \text{ kg/m}^3)$				
	$z(1) = 0.0000$	$z(1) = 0.2311$	$z(1) = 0.5392$	$z(1) = 0.7855$	$z(1) = 0.9210$		$z(1) = 0.0000$	$z(1) = 0.2311$	$z(1) = 0.5392$	$z(1) = 0.7855$	$z(1) = 0.9210$
$T = 323.20 \text{ K}$											
5.00	0.64345					25.00	0.66754		0.54351	0.45407	0.43553
7.50	0.64697		0.48935			27.50	0.66988		0.54802	0.46186	0.44315
9.90			0.50149	0.36017	0.33856	29.50			0.55159	0.46737	0.44873
10.00	0.65033					30.00	0.67220				
12.50	0.65346		0.51137	0.39025	0.37042	32.50	0.67455		0.55672	0.47481	0.45633
15.00	0.65662		0.51959	0.40932	0.39039	35.00	0.67671		0.56046	0.48064	0.46205
17.50	0.65944		0.52657	0.42370	0.40490	37.50	0.67872		0.56387	0.48569	0.46715
19.70			0.53225	0.43421	0.41558	39.30			0.56641	0.48919	0.47053
20.00	0.66216					39.50	0.68037				
22.50	0.66475		0.53817	0.44545	0.42684						
$T = 348.25 \text{ K}$											
5.00	0.61878	0.57297				25.00	0.64735	0.61050	0.51820	0.42544	0.39680
7.50	0.62289	0.57885	0.43651			27.50	0.65017	0.61376	0.52433	0.43516	0.40683
9.90		0.58469	0.45953	0.25902	0.23592	29.50		0.61652	0.52877	0.44214	0.41421
10.00	0.62704					30.00	0.65311				
12.50	0.63080	0.58960	0.47479	0.32415	0.29571	32.50	0.65550	0.62029	0.53476	0.45145	0.42370
15.00	0.63450	0.59428	0.48660	0.35978	0.33052	35.00	0.65797	0.62332	0.53964	0.45829	0.43075
17.50	0.63792	0.59870	0.49592	0.38339	0.35353	37.50	0.66043	0.62614	0.54397	0.46465	0.43732
19.70		0.60230	0.50337	0.39883	0.36897	39.30		0.62876	0.54672	0.46861	0.44150
20.00	0.64128					39.50	0.66237				
22.50	0.64434	0.60671	0.51138	0.41387	0.38499						
$T = 373.15 \text{ K}$											
2.50	0.58722					22.50	0.62375	0.58347		0.39205	0.34324
5.00	0.59304	0.54019				25.00	0.62731	0.58776		0.40564	0.35847
7.50	0.59837	0.54849				27.50	0.63066	0.59189		0.41712	0.37136
10.00	0.60328	0.55580		0.20736	0.17120	30.00	0.63373	0.59572		0.42705	0.38244
12.50	0.60792	0.56239		0.27612	0.22532	32.50	0.63663	0.59933		0.43568	0.39206
15.00	0.61222	0.56846		0.32415	0.26868	35.00	0.63956	0.60283		0.44342	0.40070
17.50	0.61631	0.57372		0.35404	0.30039	37.50	0.64230	0.60616		0.45057	0.40865
20.00	0.62013	0.57887		0.37541	0.32451	39.50	0.64442	0.60850		0.45570	0.41422
$T = 398.15 \text{ K}$											
2.50	0.55739					22.50	0.60341	0.55999		0.36374	0.30428
5.00	0.56530	0.50286				25.00	0.60770	0.56515		0.37982	0.32246
7.50	0.57225	0.51505				27.50	0.61129	0.57002		0.39292	0.33712
10.00	0.57865	0.52521		0.16723	0.13828	30.00	0.61501	0.57459		0.40476	0.35054
12.50	0.58447	0.53392		0.22916	0.18234	32.50	0.61822	0.57874		0.41461	0.36193
15.00	0.58972	0.54147		0.28222	0.22222	35.00	0.62163	0.58290		0.42366	0.37232
17.50	0.59477	0.54840		0.31799	0.25588	37.50	0.62468	0.58653		0.43174	0.38120
20.00	0.59914	0.55438		0.34361	0.28234	39.50	0.62703	0.58943		0.43753	0.38773

Table 14. Density ρ of Propane (1) + Methanol (2) + Carbon Dioxide (3) Compressed Liquid Mixtures as a Function of Pressure P and Mole Fractions $z(1)$ and $z(2)$ at Temperature T

$P/(\text{MPa})$	$\rho/(10^3 \text{ kg/m}^3)$				$P/(\text{MPa})$	$\rho/(10^3 \text{ kg/m}^3)$			
	$z(1) = 0.0534$ $z(2) = 0.8812$	$z(1) = 0.2600$ $z(2) = 0.6558$	$z(1) = 0.5534$ $z(2) = 0.2845$	$z(1) = 0.2001$ $z(2) = 0.3967$		$z(1) = 0.0534$ $z(2) = 0.8812$	$z(1) = 0.2600$ $z(2) = 0.6558$	$z(1) = 0.5534$ $z(2) = 0.2845$	$z(1) = 0.2001$ $z(2) = 0.3967$
$T = 323.20 \text{ K}$									
2.50		0.64444			22.50	0.77098	0.68192	0.59454	0.72413
5.00	0.74960	0.65037	0.54017		25.00	0.77357	0.68530	0.59953	0.73139
7.50	0.75307	0.65588	0.55159		27.50	0.77606	0.68866	0.60425	0.73806
9.90	0.75592	0.66039	0.56033	0.66412	29.50	0.77805	0.69115	0.60776	0.74296
12.50	0.75921	0.66537	0.56896	0.68333	32.50	0.78083	0.69474	0.61247	0.74968
15.00	0.76231	0.66980	0.57629	0.69601	35.00	0.78320	0.69746	0.61649	0.75497
17.50	0.76537	0.67408	0.58295	0.70680	37.50	0.78537	0.70047	0.62029	0.76003
19.70	0.76776	0.67764	0.58831	0.71498	39.30	0.78702	0.70270	0.62304	0.76353

Table 14. (Continued)

P/(MPa)	$\rho/(10^3 \text{ kg/m}^3)$				P/(MPa)	$\rho/(10^3 \text{ kg/m}^3)$			
	z(1) = 0.0534 z(2) = 0.8812	z(1) = 0.2600 z(2) = 0.6558	z(1) = 0.5534 z(2) = 0.2845	z(1) = 0.2001 z(2) = 0.3967		z(1) = 0.0534 z(2) = 0.8812	z(1) = 0.2600 z(2) = 0.6558	z(1) = 0.5534 z(2) = 0.2845	z(1) = 0.2001 z(2) = 0.3967
<i>T</i> = 348.20 K									
5.00	0.72112	0.61300			25.00	0.74956	0.65809	0.56720	
7.50	0.72503	0.62045	0.49659		27.50	0.75222	0.66205	0.57304	
9.90	0.72891	0.62743	0.51239		29.50	0.75449	0.66518	0.57749	
12.50	0.73300	0.63341	0.52559		32.50	0.75785	0.66946	0.58360	
15.00	0.73643	0.63918	0.53630		35.00	0.76037	0.67272	0.58827	
17.50	0.73986	0.64429	0.54537		37.50	0.76282	0.67611	0.59274	
19.70	0.74273	0.64878	0.55255		39.30	0.76483	0.67841	0.59587	
22.50	0.74637	0.65354	0.56065						
<i>T</i> = 373.15 K									
2.50					22.50	0.72025	0.61552	0.52359	
5.00	0.68964				25.00	0.72382	0.62132	0.53203	
7.50	0.69475	0.56129			27.50	0.72724	0.62666	0.53966	
10.00	0.69952	0.57500	0.45106		30.00	0.73043	0.63160	0.54636	
12.50	0.70417	0.58534	0.47339		32.50	0.73362	0.63624	0.55272	
15.00	0.70856	0.59420	0.48986		35.00	0.73652	0.64065	0.55842	
17.50	0.71265	0.60223	0.50299		37.50	0.73939	0.64471	0.56387	
20.00	0.71652	0.60921	0.51407		39.50	0.74165	0.64790	0.56810	
<i>T</i> = 398.15 K									
5.00	0.65358				25.00	0.69617	0.58928	0.49425	
7.50	0.66048				27.50	0.70010	0.59563	0.50397	
10.00	0.66673	0.52479			30.00	0.70391	0.60190	0.51248	
12.50	0.67244	0.54168	0.40729		32.50	0.70755	0.60740	0.52024	
15.00	0.67786	0.55445	0.43457		35.00	0.71098	0.61269	0.52731	
17.50	0.68289	0.56508	0.45457		37.50	0.71435	0.61759	0.53390	
20.00	0.68755	0.57416	0.47021		39.50	0.71705	0.62160	0.53888	
22.50	0.69200	0.58219	0.48329						

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